



# Variable Fluid Properties and Partial Slip Effect of MHD Flow of Nanofluids over a permeable Stretching Sheet with Heat Radiation and Viscous Dissipation

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**Abstract:** The simultaneous effects of variable fluid properties and velocity slip on a nanofluid flow over a continuously stretching semi-infinite horizontal sheet are investigated. The contribution of thermal radiation term is taken into account in the temperature equation. Viscous dissipation, Brownian motion and thermophoresis effects are taken into account. The flow is subjected to a transverse uniform magnetic field. Thermal conductivity and fluid viscosity are assumed to related linearly and inversely linear with temperature, respectively. The system of equations governed the problem is transformed into a dimensionless system of ordinary differential equations. This system is solved using shooting technique in conjunction with Rung-Kuta method. Convergence of the obtained solutions is examined. It is found that the velocity improved due to increasing  $\theta_r$ , whereas increasing  $t_v$  yields to decrease the velocity. Increasing volume fraction parameter  $\phi$  and nanolayer thickness  $t_v$  tend to reduce the temperature. We discuss in detail the effect of involved parameters on the velocity, temperature, and concentration profiles. In addition, we provide discussions and tabulated data on skin friction, Nusselt number, and Sherwood numbers.

**Keywords:** MHD; Nanofluids; thermal radiation; variable fluid properties; viscous dissipation.

**2010 Mathematics Subject Classification. ;**

## 1 Introduction

Convection heat transfer in a fluid flow past a semi-infinite permeable continuously stretching surface nestled in a porous medium is of great importance due to its huge range of applications in industrial, environmental and engineering. P.S.Gupta and A.S.Gupta [1] investigated the suction and blowing effect on heat and mass transfer near a stretching sheet. Shanshan Yao et al. [2] derived the convective boundary condition effect on the boundary layer of a generalized stretching/shrinking wall. Liancun Zheng et al. [3] analyzed the time dependent flow and heat transfer with heat source or sink over a permeable stretching wall. The forced convection flow of a Jeffrey fluid past a continuously stretching plate was studied by Nemat Dalir [4]. Nanotechnology deals with the manipulation and control of materials with volume at 1 to 100 nanometers. The behavior of a material nano-particles differs from their behavior at a larger scale. Nanofluid is one of the most interesting applications of nanotechnology that has revolutionized various industries, including electronics, medicine, energy, and materials science. Choi et al. [5] is the first who introduced the word nanofluid. Magneto-hydrodynamics flow of a Nanofluid attract the attention of many researchers such as Hamad [6] who presented a solution of the MHD free convective flow of a nanofluid. The effect of stagnation-point on MHD heat transfer past a stretching surface was studied by many researchers. M. Turkey ilmazoglu and I. Pop [7] studied the stagnation point on the heat transfer of a Jeffrey fluid flow past a continuously stretching plate. F. M. Ali et al. [8], G.K. Ramesh et al. [9] studied the problem with non-uniform source/sink. N. S. Akbar et al. [10] studied the heat transfer of Prandtl fluid past a shrinking plate. Behrouz Raftari and K.Vajravelu [11] presented numerical solution for the problem of MHD fluid flow in a stretchable wall channel using homotopy method. Umar Khan et al. [12] investigated stagnation point flow of a MHD nanofluid with thermal diffusing near a stretching sheet. Rana and Bhargava [13] used finite difference method to

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derive heat transfer of a nanofluid flow near a nonlinearly stretching surface. For more researches deal with this problem, see the following references [14,15,16]. Jaber [17] investigated the simultaneous effects of Hall currents and heat radiation on MHD flow of a fluid with variable properties near a vertical plate stretched uniformly. Due to the important role of viscous dissipation in processes subjected to big contrast of gravitational force, viscous dissipation has attracted the attention of many researchers. Fluid of variable properties considering viscous dissipation also studied by Tasawar Hayat et al. [18] and Jaber [19] who take into account the joule heating on MHD flow past a stretching vertical plate. Mohsen Sheikholeslami and Davood Domiri Ganji [20] considered the heat transfer of a nanofluid flow between parallel plates. S. A. Shehzad et al. [21] examined Newtonian heating and viscous dissipation effect on the third grade nanofluid flow. Swati Mukhopadhyay [22] studied the heat transfer past a wall stretched exponentially and embedded in a thermally stratified medium. For more reading in thermal radiation and variable fluid properties, see the following reference [23,24,25,26,27]. Shrivani et al. [28] used Keller box numerical method to derive nanofluid flow. Swati Mukhopadhyay [29] studied slip effects, suction/blowing and thermal radiation on flow past a wall stretched exponentially. Wubshet Ibrahim and Bandari Shankar [30] consider the thermal, velocity and melt slip conditions on MHD nanofluid flow over a permeable stretching sheet. T. Hayat et al. [31] investigated hall current, ionslip and Joule heating effects on peristaltic nanofluid flow. Jawad Raza et al. [32] derived heat and mass transfer of MHD nanofluid flow with slip effect in a rotating channel. Radiation and Joule heating effects on micropolar fluid was considered by M. Ramzan et al. [33]. Partial slip effect was studied by Tasawar Hayat et al. [34] who considered Ferro-fluid flow past rotating stretchable disks, Aminreza Noghrehabadi et al. [35] who considered nanofluid flow past continuously stretching surface and Das [36] who derived the flow past non-linearly moving sheet.

When large temperature differences and radiative heat transfer are encountered, the fluid properties deviate from stability, which makes Boussinesq's approximation inapplicable. Thus, researchers have gone deeper into exploring the effect of these factors on fluid flow behavior and heat transfer.

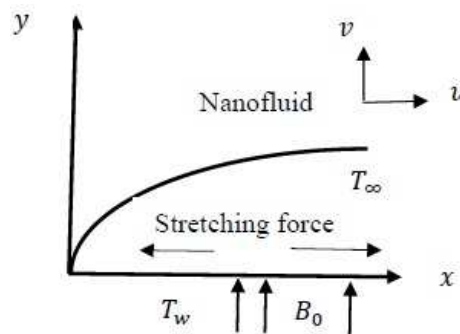


Fig. 1: Physical model and coordinate.

## 2 Mathematical Formulation

We consider a laminar steady state slip flow of a nanofluid over a permeable continuously stretching sheet. The fluid properties are taken to vary as follows. The thermal conductivity and temperature related linearly, while the fluid viscosity varies linearly with the reciprocal of the temperature. We considered the size and volume of nanoparticles, volume fraction and nanolayer, the viscous dissipation and heat radiation. We assume that the sheet slip velocity to be a constant multiple of  $x$ , the wall velocity is  $u_w = ax$ . A magnetic field with a uniform strength  $B_0$  is applied transversely to the plate. Due to the small magnetic Reynolds number, we did not take the induced magnetic field into account. The  $x$ -axis is taken along the plate in the direction of flow, the  $y$ -axis perpendicular to it. The tangential and normal fluid velocities are  $u$  and  $v$ , respectively.

The continuity equation, the momentum equation, the energy equation and the concentration equation governing the problem under consideration are written as:

$$\frac{\partial(\rho u)}{\partial x} + \frac{\partial(\rho v)}{\partial y} = 0, \quad (1)$$

$$\rho_{nf} \left( u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = \frac{\partial}{\partial y} \left( \mu(T) \frac{\partial u}{\partial y} \right) - \sigma B_0^2 u - \frac{\mu_{nf}}{K'} u, \quad (2)$$

$$(\rho C)_{nf} \left( u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \right) = \frac{\partial}{\partial y} \left( K(T) \frac{\partial T}{\partial y} \right) + (\rho C)_p \left( D_B \frac{\partial C}{\partial y} \frac{\partial T}{\partial y} + \frac{D_T}{T_\infty} \left( \frac{\partial T}{\partial y} \right)^2 \right) + \mu_{nf} \left( \frac{\partial u}{\partial y} \right)^2 - \frac{\partial q_r}{\partial y}, \quad (3)$$

$$\left( u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} \right) = D_B \frac{\partial^2 C}{\partial y^2} + \frac{D_T}{T_\infty} \frac{\partial^2 T}{\partial y^2}. \quad (4)$$

The associated boundary conditions:

$$u = \delta u_w(x) + u_s, v = v_w(x), -k_f \frac{\partial T}{\partial y} = h(T_w - T_\infty), \quad C = C_w \text{ as } y = 0 \quad (5)$$

$$y = 0 \rightarrow u \rightarrow 0, v \rightarrow 0, T \rightarrow T_\infty, C \rightarrow C_w \text{ as } y \rightarrow \infty$$

Where  $D_B = \frac{KTC}{3\pi\mu d_p}$  and  $u_w(x), v_w(x)$  are the horizontal and vertical components of the variable velocity. The suction represented when  $v_w(x) < 0$ , while  $v_w(x) > 0$  represents injection.

The fluid viscosity assumed as Ling and Dybbs [37] suggested of the form

$$\frac{1}{\mu} = \frac{1 + \gamma(T - T_\infty)}{\mu_\infty} = a(T - T_r). \quad (6)$$

Where the value of the constants  $a = \frac{\gamma}{\mu_\infty}$  and  $T_r = T_\infty - \frac{1}{\gamma}$  depend on a reference state. In general,  $a > 0$  for liquid and  $a < 0$  for gasses. The constants  $\mu_\infty, \gamma$  and  $T_\infty$  are the dynamic viscosity, the fluid thermal property and fluid temperature away from the plate, respectively. The linear relation between thermal conductivity and temperature according to [37] is written as

$$K(T) = k_{nf} [1 + \varepsilon\theta]. \quad (7)$$

Here  $\varepsilon$  is the thermal conductivity factor. According to Rosseland approximation the radiation can be written as

$$q_r = -\frac{4\sigma^*}{3K^*} \frac{\partial T^4}{\partial y}. \quad (8)$$

Where  $K^*$  is the absorption coefficient. The temperature difference is expanded as a Taylor series of  $T^4$  about  $T_\infty$  neglecting higher orders as

$$T^4 \cong 4T_\infty^3 T - 3T_\infty^4. \quad (9)$$

The density of the nanofluid taking into consideration the base fluid density, the size and volume of nanoparticles, volume fraction and nanolayer according to Mohsen Sharifpur [38] is given as:

$$\rho_{nf} = \frac{(1 - \phi)\rho_f + \phi\rho_p}{(1 - \phi) + \left(1 + \frac{t_v}{r_p}\right)^3}, \quad (10)$$

the approximation of the nanolayer thickness  $t_v$  according to Mohsen Sharifpur [38] and  $\mu_{nf}$  are given by:

$$t_v = -0.0002833r_p^2 + 0.0475r_p - 0.1417, \quad (11)$$

where the average effective size of  $Fe_3O_4$  particle in range of 21-123 nm, and the average effective size of  $Al_2O_3$  particle size 39.1 nm. Also,

At constant pressure the nanofluid thermal conductivity and the specific heat  $k_{nf}, (C_p)_{nf}$  respectively with reference to [39] are given by

$$(\rho C_p)_f = (1 - \phi)(\rho C_p)_{nf} + \phi(\rho C_p)_s, \quad \frac{k_{nf}}{k_f} = \frac{k_s + 2k_f - 2\phi(k_f - k_s)}{k_s + 2k_f + \phi(k_f - k_s)}. \quad (12)$$

To non-dimensionalize the governing equations we introduce the following non dimensional variables and similarity transform:

$$\eta = y \sqrt{\frac{C(n+1)}{2\nu_f}} x^{\frac{n-1}{2}}, \quad \psi = \rho \sqrt{\frac{2C\nu_f}{n+1}} x^{n+1} f(\eta), \quad \theta(\eta) = \frac{T - T_\infty}{T_w - T_\infty}, \quad \phi(\eta) = \frac{C - C_\infty}{C_w - C_\infty}.$$

Where the stream function  $\psi$  satisfies the continuity equation so,  $\frac{\partial \psi}{\partial y} = \rho u$  and  $\frac{\partial \psi}{\partial x} = -\rho v$ . Then the dimensionless temperature  $\theta(\eta)$  can be written as

$$\theta(\eta) = \frac{T - T_r}{T_w - T_\infty} + \theta_r, \quad (13)$$

where  $\theta_r = \frac{T_r - T_\infty}{T_w - T_\infty}$ . Using this formula equation (6) can be written as

$$\mu_{nf} = \frac{\mu_f \theta_r}{\theta_r - \theta}. \quad (14)$$

Executing the previous similarity variables, we get:

$$u = cx^n f', v = -\sqrt{\frac{c(n+1)v_f}{2}} x^{\frac{n-1}{2}} \left( f + \frac{n-1}{n+1} \eta f' \right). \quad (15)$$

In view of the previous dimensionless quantities Equations (1) (4) reduced to the following system of non-dimensional ordinary differential equations

$$\left( 1 - \phi + \phi \frac{\rho_p}{\rho_f} \right) \left( \frac{2n}{n+1} f'^2 - f f'' - \frac{\theta_r}{\theta_r - \theta} \left( f''' + \frac{1}{\theta_r} f'' \right) \right) + \left( 1 - \phi + \phi \left( 1 + \frac{t_v}{r_p} \right)^3 \right) \left( M + \frac{\theta_r}{\theta_r - \theta} k \right) f' = 0, \quad (16)$$

$$\frac{k_{nf}}{k_f} \frac{1}{Pr} \left( \varepsilon \theta'^2 + (1 + \varepsilon \theta) \theta'' \right) + [(1 - \phi) + \tau \phi] f \theta' + (N_b \theta' \phi' + N_t \theta'^2) + \frac{\theta_r}{\theta_r - \theta} Ec f'^2 - 4R \theta'' = 0, \quad (17)$$

$$f' \phi' + Sc \phi'' + Sr \theta'' = 0. \quad (18)$$

Where prime denotes differentiation with respect to  $\eta$ ,  $M = \frac{\sigma B_0^2 x}{\rho u_w}$  is the magnetic number,  $k = \frac{2v_f x}{K u_w (n+1)}$  is Porosity parameter,  $Ec = \frac{u_w^2}{(T_w - T_\infty)(C_p)_f}$  is the Eckert number,  $N_b = \frac{(\rho C_p)_f D_B (C_w - C_\infty)}{(\rho C_p)_{nf} v_f}$ ,  $N_t = \frac{(\rho C_p)_f D_T}{(\rho C_p)_{nf} T_\infty v_f} (T_w - T_\infty)$  are the Brownian motion and thermophoresis parameters,  $Sr = \frac{D_B K_T (T_w - T_\infty)}{T_m v (C_w - C_\infty)}$  is the Soret coefficient and  $Sc = \frac{D_B}{v}$  is the Schmidt number. The non-dimensional fluid viscosity parameter  $\theta_r$  and the thermal radiation parameter  $R$  are given by

$$\theta_r = \frac{T_r - T_\infty}{T_w - T_\infty} = \frac{-1}{\gamma(T_w - T_\infty)}, \quad R = \frac{4\sigma^* T_\infty^3}{3\mu C_p k^*}. \quad (19)$$

$\theta_r$  is determined by thermal property of the fluid and temperature differences. Variable viscosity has a significant effect in case of large temperature differences, so small values of  $\theta_r$  will be considered. The boundary conditions are transformed to the following non-dimensional form

$$f = S, f'(0) = \chi + \lambda f''(0), \theta'(0) = -\beta(1 - \theta(0)), f'(\eta) = \theta(\eta) = \phi(\eta) = 0 \text{ as } \eta \rightarrow \infty. \quad (20)$$

Where  $S = \frac{-v_w}{v_f} \left[ \frac{c(n+1)x^{n-1}}{2} \right]^{-\frac{1}{2}}$ ,  $\beta = \frac{h}{k_f} \left[ \frac{c(n+1)x^{n-1}}{2v_f} \right]^{-\frac{1}{2}}$ .

The physically important quantities namely, the skin friction coefficient which is the resistant force acting on a particle moving in a fluid, Nusselt number and Sherwood number are expressed as:

$$C_f = \frac{2\tau_w}{\rho_f u_w^2}, \quad Nu = \frac{xq_w}{k_f (T_w - T_\infty)}, \quad Sh = \frac{xq_m}{D_B (C_w - C_\infty)} \quad (21)$$

Where  $\tau_w$  is the wall shear stress,  $q_w$  is the wall heat flux,  $q_m$  is the mass flux, are given by:

$$\tau_w = \mu \frac{\partial u}{\partial y} \Big|_{y=0}, \quad q_w = -k_{nf} \frac{\partial T}{\partial y} \Big|_{y=0}, \quad q_m = -D_B \frac{\partial \phi}{\partial y} \Big|_{y=0}. \quad (22)$$

Based on equations (21) and (22) the non-dimensional skin friction coefficient is expressed as

$$C_f = \frac{2\mu}{\rho_f u(x)^2} \frac{\partial u}{\partial y} \Big|_{y=0} = \sqrt{\frac{2x^{n-1}(n+1)v_f}{c}} \frac{\mu_{nf}}{\mu_f} f''(0). \quad (23)$$

The Nusselt number is given by

$$Nu = \frac{-k_{nf}x}{k_f(T_w - T_\infty)} \frac{\partial T}{\partial y} \Big|_{y=0} = -\sqrt{\frac{c x^{n-1} (n+1)}{2\nu_f} \frac{K_{nf}}{K_f}} \theta' (0). \tag{24}$$

Sherwood number is expressed as:

$$Sh = -\sqrt{\frac{c x^{n+1} (n+1)}{2\nu_f}} \phi' (0). \tag{25}$$

Model	$C_p(Kg^{-1}K^{-1})$	$\rho(Kgm^{-3})$	$k(Wm^{-1}K^{-1})$
$H_2O$	4179	997.1	0.613
$Al_2O_3$	765	3970	40
$Fe_3O_4$	670	5180	9.7

**Table 1:** Thermo-physical properties of the water (base fluid) and nanoparticles ( $Al_2O_3$  and  $Fe_3O_4$ ) (see [40]).

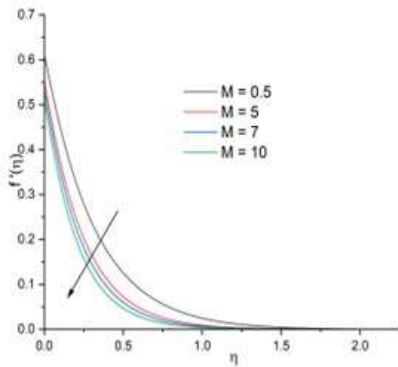
### 3 Solution Scheme

The system of ordinary differential equations and boundary conditions (16)–(18) is solved to investigate the effect of all involved parameters numerically using Mathematica software to run the 4th order Runge-Kutta algorithm by shooting technique. To investigate the effect of the parameters under study, we fixed the parameter values  $\theta_r = 1.2$ ,  $R = 0.1$ ,  $\varphi = 0.01$ ,  $t_v = 0.01$ ,  $Sr = 0.2$ ,  $Pr = 0.72$ ,  $Ec = 0.1$ ,  $n = 0.1$  during the calculations and took different values for the parameter under consideration. To ensure convergence in the calculations, a criterion that the difference between any two consecutive iterations is less than  $10^{-9}$  is employed.

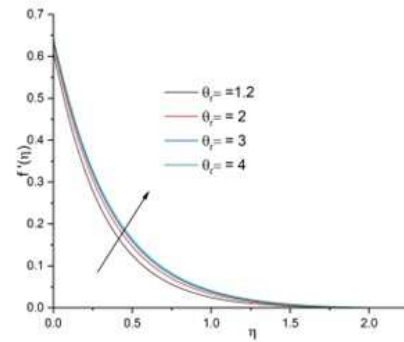
### 4 Results And Discussions

The effect on velocity, heat transfer and mass transfer is presented graphically, the effect on skin friction, Nusselt number and Sherwood number is tabulated.

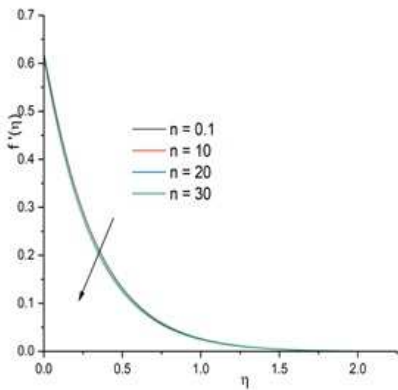
Figure 2 shows the effect of the Magnetic Number  $M$  on the flow velocity within the boundary layer. It is seen that increasing the magnetic number  $M$  decreases the dimensionless velocity  $f'$ . Figure 3 established the influence of the fluid viscosity parameter  $\theta_r$ . It is seen that the fluid velocity increases with increasing values of  $\theta_r$ . This behavior due to fact that the increasing in  $\theta_r$  actually yields to decrease the dynamic viscosity as obvious from expression (14) so the fluid velocity will increase. Figure 4 shows the impact of the power index parameter  $n$ , it is clear that increasing  $n$  decreases the velocity. While it is evident from Figure 5 that the temperature decreases with an increase in values of  $R$  the thermal radiation parameter. Figure 6 plotted to study the effect of Eckert number on temperature transfer profile. It is perceived that increasing Eckert number significantly increases temperature transfer. Figure 7 reveals that the temperature transfer decreases due to increasing Prandtl number  $Pr$ . Figure 8 reveals that mass transfer enhanced due to the increase in the Sherwod number.



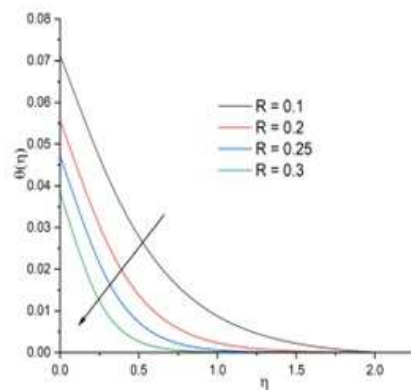
**Fig. 2:** Effect of  $M$  on the velocity profiles with  $\theta_r = 1.2, R = 0.1, \varphi = 0.01, t_v = 0.01, Sr = 0.2, Pr = 0.72, Ec = 0.1, n = 0.1$ .



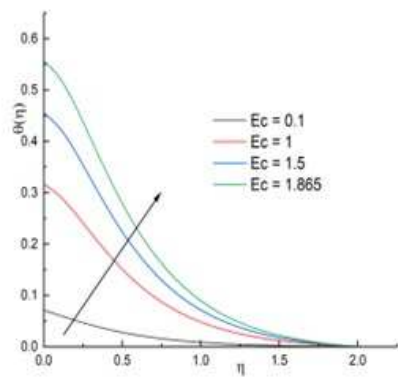
**Fig. 3:** Effect of  $\theta_r$  on velocity profiles with  $M = 0.5, R = 0.1, \varphi = 0.01, t_v = 0.01, Sr = 0.2, Pr = 0.72, Ec = 0.1, n = 0.1$ .



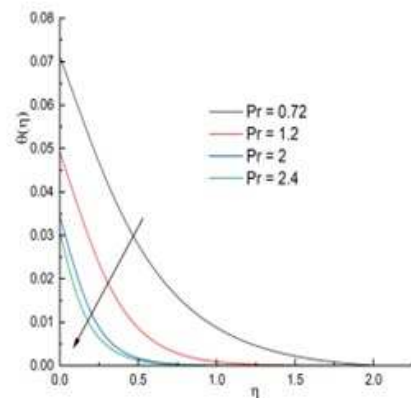
**Fig. 4:** Effect of  $n$  on velocity profiles with  $\theta_r = 1.2, R = 0.1, \varphi = 0.01, t_v = 0.01, Sr = 0.2, Pr = 0.72, Ec = 0.1, n = 0.1, M = 0.5$ .



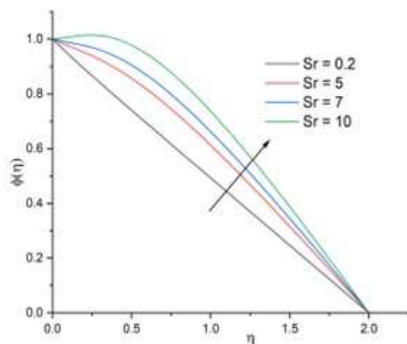
**Fig. 5:** Effect of  $R$  on temperature profiles with  $\theta_r = 1.2, R = 0.1, \varphi = 0.01, t_v = 0.01, Sr = 0.2, Pr = 0.72, Ec = 0.1, n = 0.1, M = 0.5$ .



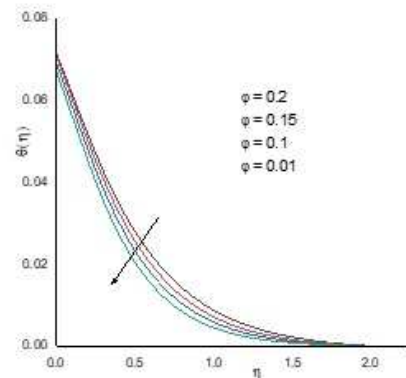
**Fig. 6:** Effect of  $Ec$  on temperature profiles with  $\theta_r = 1.2, R = 0.1, \varphi = 0.01, t_v = 0.01, Sr = 0.2, Pr = 0.72, n = 0.1, M = 0.5$ .



**Fig. 7:** Effect of  $Pr$  on temperature profiles with  $\theta_r = 1.2, R = 0.1, \varphi = 0.01, t_v = 0.01, Sr = 0.2, Ec = 0.1, n = 0.1, M = 0.5$ .

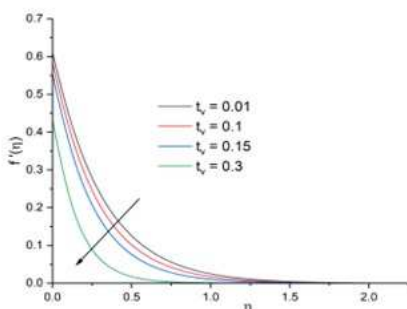


**Fig. 8:** Effect of  $Sr$  on concentration profiles with  $\theta_r = 1.2, R = 0.1, \varphi = 0.01, t_v = 0.01, Pr = 0.72, Ec = 0.1, n = 0.1, M = 0.5$ .

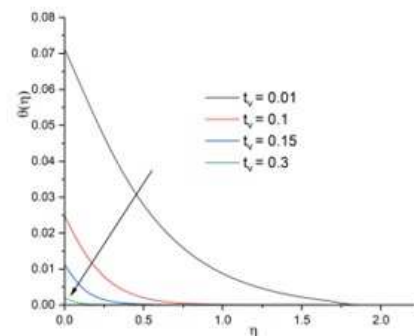


**Fig. 9:** Effect of  $\varphi$  on temperature profiles with  $\theta_r = 1.2, R = 0.1, t_v = 0.01, Sr = 0.2, Pr = 0.72, Ec = 0.1, n = 0.1, M = 0.5$ .

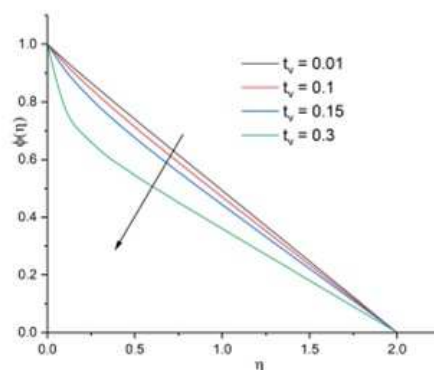
Figure 9 shows that the temperature transfer decreases by increasing  $\varphi$ . Figures 10–12 demonstrate the influence of the nanolayer thickness  $t_v$ . The impression of rising  $t_v$  has the same effect to decrease the velocity, temperature and concentration profiles. By comparing Figure 11 with Figures 10 and 12 it is clearly that nanolayer thickness  $t_v$  has greater effect in reducing fluid temperature.



**Fig. 10:** Effect of  $t_v$  on velocity profiles with  $\theta_r = 1.2, R = 0.1, \varphi = 0.01, Sr = 0.2, Pr = 0.72, Ec = 0.1, n = 0.1, M = 0.5$ .



**Fig. 11:** Effect of  $t_v$  on temperature profiles with  $\theta_r = 1.2, R = 0.1, \varphi = 0.01, Sr = 0.2, Pr = 0.72, Ec = 0.1, n = 0.1, M = 0.5$ .



**Fig. 12:** Effect of  $t_v$  on concentration profiles with  $\theta_r = 1.2, R = 0.1, \varphi = 0.01, Sr = 0.2, Pr = 0.72, Ec = 0.1, n = 0.1, M = 0.5$ .

The effect of viscosity/temperature parameter  $\theta_r$ , thermal radiation parameter  $R$ , Volume fraction parameter  $\varphi$ , nanolayer thickness  $t_v$  and soret coefficient  $Sr$  on skin-friction coefficient  $C_f$ , Nusselt number  $Nu$  and Sherwood number  $Sh$  are tabulated and presented in table 2. The numerical computations reveals that the improvement in  $\varphi$  increases the skin friction, Nusselt and Sherwood numbers, while these numbers decrease with increasing in nanolayer thickness  $t_v$ . The increase in viscosity/temperature parameter  $\theta_r$  increases the skin friction and decreases Nusselt and Sherwood numbers. High thermal radiation parameter  $R$  and soret number  $Sr$  have the same effect in reducing Nusselt and Sherwood numbers and to increase skin friction coefficient.

$\theta_r$	$R$	$\varphi$	$t_v$	$Sr$	$f''(0)$	$-\theta'(0)$	$-\phi'(0)$
1.2	0.1	0.01	0.01	0.2	-1.9608	0.092759	0.564379
2	0.1	0.01	0.01	0.2	-1.86046	0.09291	0.57281
3	0.1	0.01	0.01	0.2	-1.8105	0.09298	0.5771
1.2	0.2	0.01	0.01	0.2	-1.95997	0.09443	0.5623
1.2	0.3	0.01	0.01	0.2	-1.96989	0.09616	0.5597
1.2	0.1	0.15	0.01	0.2	-1.9496	0.09333	0.54969
1.2	0.1	0.2	0.01	0.2	-1.94801	0.09312	0.55271
1.2	0.1	0.2	0.15	0.2	-2.23533	0.09887	1.01484
1.2	0.1	0.01	0.3	0.2	-2.84538	0.099805	3.91634
1.2	0.1	0.01	0.01	7	-1.95065	0.092908	0.163023
1.2	0.1	0.01	0.01	10	-1.95072	0.092922	-0.014969

**Table 2:** Variation of skin friction, Nusselt number and Sherwood number with  $\theta_r$ ,  $R$ ,  $\varphi$  and  $t_v$

## 5 Conclusion and Remarks

The study derived the simultaneous effects of variable fluid properties on laminar steady state slip of a nanofluid flow past a permeable continuously stretching sheet. The flow passes through a uniform transverse magnetic field of strength  $B_0$ . The relation between thermal conductivity and temperature is considered linear, whereas the relation between fluid viscosity and temperature is assumed to be inversely linear. We assume the sheet slip velocity as a constant multiple of  $x$ ,  $u_w = ax$ . To obtain accurate results, the density of the base fluid, the size and volume of the nanoparticles, the volume fraction and the nanoscale are taken into account to estimate the density of variable fluids. Using appropriate non-dimensional quantities and boundary layer assumptions the equations of the mathematical modeling non-dimensionalized then solved numerical using 4<sup>th</sup> order Runge Kutta by shooting.

The computations shown that the flow velocity improved due to the increase in viscosity/temperature parameter  $\theta_r$ , whereas growing Power index parameter  $n$  and nanolayer thickness  $t_v$  tend to depress the velocity. the temperature transfer increased due to the increase in Eckert number  $Ec$ . While the improvement in thermal radiation parameter  $R$ , Prandtl number  $Pr$ , Volume fraction parameter  $\varphi$  and nanolayer thickness  $t_v$  tend to reduce the temperature. the concentration improved due to the increase in soret number  $Sr$ . Growing  $t_v$  tend to reduce the concentration. the skin friction increased due to growing  $\theta_r$  and  $\varphi$ , whereas it is decreased due to the increase in  $R$ , soret number  $Sr$ , and  $t_v$ . the Nusselt number decreased owing to the increase in  $R$ , soret number  $Sr$ , and  $t_v$ , whereas it is increased due to the increase in  $\varphi$ . the Sherwood number  $Sh$  increased by the growing of the values  $R$ , soret number  $Sr$ , whereas it is decreased owing to the increased in  $\theta_r$  and  $\theta_r$ .



## Nomenclature

$B_0$	Constant magnetic field	$X$	Streamwise coordinate
$c$	Constant	<b>Greek Symbols</b>	
$C$	Concentration	$\delta$	Stretching/shrinking parameter
$C_f$	Coefficient of skin friction	$\varepsilon$	Thermal conductivity factor
$C_p$	Specific heat at constant pressure	$\phi$	Dimensionless concentration
$D_T$	Thermodiffusion coefficient	$\eta$	Pseudo similar variable
$Ec$	Eckert number	$\varphi$	Volume fraction parameter
$f$	Dimensionless stream function	$\mu$	Dynamical viscosity
$g$	Gravity acceleration	$\nu$	Kinematical viscosity
$Gr$	Grashof number	$\theta$	Dimensionless temperature
$K$	thermal conductivity	$\theta_r$	Viscosity/temperature parameter
$N$	Power index parameter	$\rho$	Density
$Nu$	Nusselt number	$\sigma$	Stefan-Boltzmann constant
$Pr$	Prandtl number	$\tau$	Shearing stress
$r$	Radius	$\psi$	Stream function
$S$	Heat source/sink parameter	<b>Subscripts</b>	
$Sc$	Schmidt number	$f$	Base fluid
$Sr$	soret coefficient	$nf$	nanofluid
$t_v$	Nanolayer thickness	$p$	Solid particles
$u$	Flow velocity in x-direction	$W$	property at the wall
$u_s$	Slip velocity	$\infty$	freestream condition
$v$	Flow velocity in y-direction	<b>Superscripts</b>	
$T$	Temperature	'	differentiation with respect to $\eta$ only

## Declarations

**Competing interests:** The author declares no competing interests.

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